# THERMAL ANALYSIS AND KINETICS OF OXIDATION OF "NbS<sub>2</sub>"

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The thermal analysis and kinetics of oxidation of " $NbS_2$ " to  $Nb_2O_5$  were studied by thermogravimetry. The application of both isothermal and nonisothermal methods was necessary to establish the correct equation

 $1-(1-\alpha)^{1/3} = kt$ 

This equation was valid for the reaction of sample reacted  $\alpha$  in the interval 0.03 to 0.82–0.91. The apparent activation energy was determined to be 209.59 ± 2.36 kJ mol<sup>-1</sup> with the isothermal method and 209.28 ± 1.84 kJ mol<sup>-1</sup> with the nonisothermal method (5 deg min<sup>-1</sup>) over the  $Po_2$  range  $8.9 \times 10^{-2}$  to  $2.0 \times 10^{-1}$  atm and the temperature range 440 to 515°. The relationship between the rate constant k and  $Po_2$  was also determined.

We earlier reported the kinetics of oxidation of vanadium and titanium sulfides [1, 2]. Factors which influence the kinetic parameters were discussed, and it was shown that experiments should be carried out in an appropriate range of oxygen partial pressure  $(Po_2)$  to obtain realistic values of apparent activation energy E and preexponential factor A.

Tatsuki et al. [3] in our laboratory established the phase relations in the Nb-S system at high temperature. However no work has yet been done on the thermal analysis and kinetics of oxidation of niobium sulfide.

Until recently, mainly the isothermal method was used for kinetic studies. With the development of the methods and appropriate mathematical models [4], dynamic methods have become popular, since they are less tedious and also time-saving, and the results obtained with the two methods do not differ significantly [5–9]. Consequently, many investigators prefer to use the dynamic method alone. It will be shown in this paper, however, that there are cases such as the oxidation of niobium sulfide where it is essential to use both methods to demonstrate the correct mechanism clearly.

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### Experimental

### Method

The TG–DTA measurements were performed with a Rapid Heating Rigaku Thermoflex TG–DTA unit. Twenty, 10, 5 and 2.5 mg quantities of the sample were weighed accurately in a platinum crucible of  $2.5 \times 5$  mm diameter, distributed evenly with a pin when a small amount was used, and bedded down by tapping 2 or 3 times on a metal surface from a height of about 5 mm. An equal amount of highpurity "dead burnt"  $\alpha$ -alumina was used as the standard reference material. The controlling of  $Po_2$  by mixing  $N_2$ -air and  $N_2$ — $O_2$ , the characterization of the sample and the reaction products, and the other experimental work, were performed in the same way as described in a previous paper [10].

# Sample preparation [3]

Reagent grade Nb<sub>2</sub>O<sub>5</sub> (Wako Pure Chemical Industries Ltd., 99.9%) was taken in a mullite boat and was heated in a flow of H<sub>2</sub>S at 700° for 24 h. The sample was then quenched to room temperature, ground, and again heated in H<sub>2</sub>S at the same temperature for 24 h. The  $3s - Nb_{1+x}S_2$  phase was identified from the X-ray diffraction pattern of the finally quenched sample. The absence of the strongest peaks for Nb<sub>2</sub>O<sub>5</sub> (Cu K<sub>x</sub> 2 $\theta$  = 28.5°) and NbO<sub>2</sub> (Cu K<sub>x</sub> 2 $\theta$  = 26.1°) was confirmed. The chemical composition of the prepared sample was determined to be NbS<sub>1.692</sub> by oxidizing the disulfide completely to Nb<sub>2</sub>O<sub>5</sub> in air at 700° for 48 h. The nonstoichiometric disulfide will be denoted as "NbS<sub>2</sub>".

#### **Results and discussion**

#### Thermal analysis

The TG–DTA curves for the oxidation of "NbS<sub>2</sub>" in air and in oxygen are shown in Fig. 1. The TG curve reveals a single step of weight loss and the DTA curve shows a very strong exothermic peak. The reaction started at 440°, and the sample temperature rose sharply to over 530° and 810° in air (for more than a 5 mg quantity of the sample) and in oxygen flows, respectively. The X-ray diffraction pattern of the sample at the end of heating showed only Nb<sub>2</sub>O<sub>5</sub> peaks. The good agreement between the calculated weight loss (9.68%) and the observed weight loss (9.6%) after correcting the TG pen drift suggests that the oxidation reaction takes place as

$$NbS_{1.692} + 2.942 O_2 \rightarrow NbO_{2.5} + 1.692 SO_2$$
 (1)



Fig. 1 TG-DTA curves when heating "NbS<sub>2</sub>" in a) air and in b) oxygen (sample amount: 10 mg, 250-270 mesh; gas flow: 2 ml s<sup>-1</sup>)

The TG–DTA curves obtained by heating 2.5 mg sample at different  $Po_2$  are depicted in Fig. 2. The Figure shows that when a small amount of sample was used, the sample temperature did not rise for moderate heating rates ( $\leq 5 \text{ deg min}^{-1}$ ), even when heating was performed in an air flow. In all cases, only Nb<sub>2</sub>O<sub>5</sub> was formed as the reaction product.



Fig. 2 The TG-DTA curves when heating "NbS<sub>2</sub>" at 5 deg min<sup>-1</sup> in different P<sub>02</sub>, (sample amount: 2.5 mg, 250-270 mesh; gas flow: 2 ml s<sup>-1</sup>)

## Kinetics of oxidation

It is clear from Fig. 2 that kinetic study of the oxidation of "NbS<sub>2</sub>" according to Eq. (1) is possible at any suitable  $Po_2$  below  $2.0 \times 10^{-1}$  atm if a small amount of sample is used.

On the basis of the above results and previous experience, 2.5 mg of the sample was taken to determine the kinetic parameters. The sample was oxidized at temperatures between 440° and 515°, selected from the dynamic TG experiments. Blank experiments, with an equal amount of  $\alpha$ -alumina taken instead of the sample, were always performed for each isothermal run and to deduce the correct  $\alpha$  vs. t data. A typical  $\alpha$  vs. t plot is depicted in Fig. 3.



Fig. 3 Typical  $\alpha$  vs. t plots for the oxidation of "NbS<sub>2</sub>" at a definite  $P_{O_2}$  over the whole range of temperature examined (sample amount: 2.5 mg, 250–270 mesh; gas flow: 2 ml s<sup>-1</sup>)

Three rate equations, from among all the possible rate equations listed in an earlier paper [1], gave almost perfect straight lines when plotted against time (Figs 4a, b, c). Variation of  $Po_2$  slightly favors the rate equation plotted in Fig. 4b. The values of k, calculated from the slopes of the lines in Figs 4a, b, c, are plotted against the inverse of temperature (K) in Fig. 5. Again they gave good straight lines, and the values of E calculated from these lines were very close to one another (Table 1). As a result, selection of the appropriate rate equations were then used to calci late the values of E nonisothermally by the Coats and Redfern method (Figs 4a, b, c), and they are listed in Table 1. The best agreement between the values of E obtained with both methods was found for the equation plotted in Fig. 4b. It is clear now from this results that a three-dimensional phase boundary reaction or a contracting volume model is the right mechanism for the oxidation reaction represented by Eq. (1). This



Fig. 4a  $F(\alpha)$  vs. t plots, where  $F(\alpha)$  corresponds to unimolecular decay controlling rate equation, I isothermal method, and II Coats and Redfern's linearization plot for nonisothermal method (5 deg min<sup>-1</sup>), ( $P_{O_2}$ : 1.29 × 10<sup>-1</sup> atm, sample amount: 2.5 mg, 250–270 mesh; gas flow: 2 ml s<sup>-1</sup>)



Fig. 4b  $F(\alpha)$  vs. t plots, where  $F(\alpha)$  corresponds to three dimensional phase boundary controlling rate equation, I isothermal method, and II Coats and Redfern's linearization plot for nonisothermal method (5 deg min<sup>-1</sup>) ( $P_{O_2}$ :  $1.29 \times 10^{-1}$  atm; sample amount: 2.5 mg, 250-270 mesh; gas flow: 2 ml s<sup>-1</sup>)

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Fig. 4c  $F(\alpha)$  vs. t plots, where  $F(\alpha)$  corresponds to random nucleation and growth accompanied by ingestion of nuclei controlling rate equation, I isothermal method, and II Coats and Redfern's linearization plot for nonisothermal method (5 deg min<sup>-1</sup>), ( $P_{O_2}$ : 1.29 × 10<sup>-1</sup> atm; sample amount: 2.5 mg, 250–270 mesh; gas flow: 2 ml s<sup>-1</sup>)



Fig. 5 Arrhenius plots for all possible rate equations depicted in Figs 4a, b, c  $\Box - \ln (1-\alpha)$ ,  $\triangle [-\ln (1-\alpha)]^{1/1.5}$ ,  $\bigcirc 1-(1-\alpha)^{1/3}$ 

rate equation,  $1-(1-\alpha)^{1/3} = kt$ , is valid for values of  $\alpha$  in the interval 0.03 to 0.82–0.91. It is noticeable here however, that both methods yield almost perfect straight lines for all three rate equations, and a decision as to the correct rate equation is difficult from either of them alone. Tanaka et al. [11] encountered similar difficulties when studying the kinetics of dehydration of magnesium oxalate dihydrate and ultimately selected the rate equation by comparing the results

kt	Isothermal E, kJ/mol	Nonisothermal (5 deg/min) E, kJ/mol	
$\frac{1}{a) - \ln(1-\alpha)}$	215.84	285.39	
b) $1-(1-\alpha)^{1/3}$	212.62	210.00	
c) $[-\ln(1-\alpha)]^{1/1.5}$	210.46	186.10	

**Table 1** Activation energy, for the isothermal and nonisothermal methods, obtained for "NbS<sub>2</sub>" when using different possible kinetic equations at a  $P_{02}$  of  $1.29 \times 10^{-1}$  atm

Sample amount: 2.5 mg, 250-270 mesh

obtained with both methods. It is therefore concluded that both isothermal and dynamic methods should be applied to be sure about the correctness of the selected rate equation, and hence about the accuracies of the observed kinetic parameters.

The values of E and A determined for different  $Po_2$  are given in Table 2. These results conform to the previous findings [2] that the values of E become stable when an adequate supply of oxygen is available. The influence of the sample amount on E was also tested at a fixed  $Po_2$  ( $8.9 \times 10^{-2}$  atm). The observed values of E for different sample amounts are plotted in Fig. 6. It is seen from this Figure that, for a

Table 2 Activation energy preexponential factor for the oxidation of "NbS<sub>2</sub>" at different  $P_{O_2}$ 

P <sub>O2</sub> (atm)	Isothermal E, kJ/mol	A, 1/s	Nonisothermal (5 deg/min) <i>E</i> , kJ/mol
0.200	206.86	4.94 × 10 <sup>11</sup>	211.10
0.129	212.62	8.95 × 1011	210.00
0.089	209.29	5.42 × 1011	206.75
0.045	198.73	7.22 × 10 <sup>10</sup>	202.00

Sample amount: 2.5 mg, 250-270 mesh



Fig. 6 Variation of apparent activation energy E with sample amount at a definite  $P_{O_2}$  (sample: "NbS<sub>2</sub>", 250–270 mesh: gas flow: 2 ml s<sup>-1</sup>)

sufficient  $Po_2$ , the sample amount (up to a certain extent) does not have a very drastic effect on the observed values of E.

Figure 7 shows the plot of  $-\log k vs. -\log Po_2$ . It is seen that k varies considerably and linearly with temperature. From the slopes of these plots, the dependence of the rate constant k on  $Po_2$  ( $8.9 \times 10^{-2}$  to  $2.0 \times 10^{-1}$  atm) was calculated as  $k = c' (po_2)^{0.342 \pm 0.034}$  over the temperature range 440 to 495°.

The particle size (e.g. -250, 250-270, 325-400 mesh) had very little effect on the observed kinetic parameters in the  $Po_2$  range studied.



Fig. 7 Plots of  $-\log k$  vs.  $-\log P_{O_2}$  at different temperatures (sample: "NbS<sub>2</sub>", 250-270 mesh; gas flow: 2 ml s<sup>-1</sup>)

#### Conclusions

"NbS<sub>2</sub>" is oxidized directly to Nb<sub>2</sub>O<sub>5</sub> in accordance with NbS<sub>1.692</sub>+ 2.942 O<sub>2</sub>  $\xrightarrow{440^{\circ}}$  Nb<sub>2.5</sub>+1.692 SO<sub>2</sub>.

Both the isothermal and nonisothermal methods of analyzing TG data over wide ranges of temperature and oxygen pressure must be used to single out the correct rate equation. For "NbS<sub>2</sub>" the oxidation is controlled by a three-dimensional phase boundary reaction, or in general by the shrinking core kinetic model of spherical particles, as  $1 - (1 - \alpha)^{1/3} = kt$  were  $\alpha = 0.03$  to 0.82–0.91.

The value of *E* determined with the isothermal method is  $209.59 \pm 2.36$  kJ mol<sup>-1</sup> and that with the nonisothermal method is  $209.28 \pm 1.84$  kJ mol<sup>-1</sup> over the  $Po_2$  range  $8.9 \times 10^{-2}$  to  $2.0 \times 10^{-1}$  atm and the temperature range 440 to  $515^{\circ}$ . However, care must be taken to select the upper  $Po_2$  limit so that the sample

temperature does not rise due to any unwanted exothermic heat of reaction. The rate constant k increases smoothly with temperature, and the observed relationship between k and  $Po_2$  is

$$k = c' (Po_2)^{0.342 \pm 0.031}$$

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**Zusammenfassung** — Die thermische Analyse und die Kinetik der Oxydation von "NbS<sub>2</sub>" zu Nb<sub>2</sub>O<sub>5</sub> wurden thermogravimetrisch untersucht. Die Anwendung sowohl der isothermen als auch der nichtisothermen Methode war notwendig, um die richtige Gleichung  $1 - (1 - \alpha)^{1/3} = kt$  aufzustellen. Diese Gleichung ist gültig für Werte von  $\alpha$  (Anteil der umgesetzten Probenmenge) im Intervall von 0,03 bis 0,82–0,91. Für die scheinbare Aktivierungsenergie wurde mit der isothermen Methode ein Wert von 209,59±2,36 kJ·mol<sup>-1</sup> und mit der nicht-isothermen (5 Grad·min<sup>-1</sup>) ein Wert von 209,28±1,84 kJ·mol<sup>-1</sup> über den  $P_{02}$ -Bereich von 8,9·10<sup>-2</sup> bis 2,0·10<sup>-1</sup> atm und den Temperaturbereich von 440–515° erhalten. Auch die Abhängigkeit der Geschwindigkeitskonstante k von  $P_{02}$ wurde ermittelt.

Резюме — С помощью термогравиметрии изучен термический анализ и кинетика окисления «NbS<sub>2</sub>» до Nb<sub>2</sub>O<sub>5</sub>. Применение изотермического и неизотермического методов было вызвано необходимостью подтвердить правильность уравнения  $1 - (1 - \alpha)^{1/3} = kt$ . Данное уравнение было справедливым для реагирующего образца с  $\alpha$  в интервале от 0,03 до 0,82–0,91. Кажущаяся энергия активации, определенная изотермическим методом, была равной 209,59±2,36 кдж/моль, а неизотермическим — 209,28±1,84 кдж/моль (при температурном интервале 440–515°, нагреве 5°/мин и  $P_{O2}$  8,9 · 10<sup>-2</sup>–2,0 · 10<sup>-1</sup>). Установлена взимосвязь между константой скорости k и  $P_{O2}$ .